

FACTORS FOR UNIT CONVERSIONS

Quantity	Equivalent Values
Mass	1 kg = 1000 g = 2.20462 lb _m 1 lb _m = 16 oz = 453.593 g = 0.453595 kg
Length	1 m = 100 cm = 1000 mm = 10 ⁶ microns (μm) = 39.37 in. = 3.2808 ft = 1.0936 yd = 0.0006214 mile 1 ft = 12 in. = 1/3 yd = 0.3048 m = 30.48 cm
Volume	1 m ³ = 1000 L = 10 ⁶ cm ³ = 10 ⁶ mL = 35.3145 ft ³ = 264.17 gal = 1056.68 qt 1 ft ³ = 1728 in. ³ = 7.4805 gal = 0.028317 m ³ = 28.317 L = 28317 cm ³
Force	1 N = 1 (kg m)/s ² = 10 ⁵ dynes = 10 ⁵ (g cm)/s ² = 0.22481 lb _f 1 lb _f = 32.174(lb _m ft)/s ² = 4.4482 N = 4.4482×10 ⁵ dynes
Pressure	1 atm = 1.01325×10 ⁵ N/m ² = 1.01325×10 ⁵ Pa = 101.325 kPa = 1.01325 bars = 760 mm Hg at 0°C = 760 torr = 10.333 m H ₂ O at 4°C = 14.696 lb _f /in. ² = 14.696 psi = 33.9 ft H ₂ O at 4°C = 29.921 in. Hg at 0°C
Energy	1 J = 1 N m = 10 ⁷ ergs = 10 ⁷ dyne cm = 2.778×10 ⁻⁷ kW h = 0.23901 cal = 0.7376 ft lb _f = 9.486 ×10 ⁻⁴ Btu
Power	1 W = 1 J/s = 0.23901 cal/s = 0.7376 ft lb _f /s = 9.486×10 ⁻⁴ Btu/s = 1.341×10 ⁻³ hp
Temperature	$(T \text{ in } ^\circ\text{C}) = ((T \text{ in } ^\circ\text{F}) - 32^\circ\text{F}) / (1.8\Delta^\circ\text{F}/\Delta^\circ\text{C})$ $(T \text{ in } ^\circ\text{F}) = (T \text{ in } ^\circ\text{C})(1.8\Delta^\circ\text{F}/\Delta^\circ\text{C}) + 32^\circ\text{F}$ $(T \text{ in K}) = (T \text{ in } ^\circ\text{C}) + 273.15$ $(T \text{ in R}) = (T \text{ in } ^\circ\text{F}) + 459.67$
Electric Current	(Ampere) 1 A
Frequency	(hertz) 1 Hz = 1 s ⁻¹
Electric potential	(volt) 1 V = 1 W/A = 1 J/C
Electric resistance	(ohm) 1 Ω = V/A
Electric charge	(coulomb) 1 C = A s

Example: The factor to convert grams to lb_m is $\left(\frac{2.20462 \text{ lb}_m}{1000 \text{ g}} \right)$

Commonly Used SI Prefixes

Factor	Prefix	Symbol
10 ¹²	tera	T
10 ⁹	giga	G
10 ⁶	mega	M
10 ³	kilo	k
10 ⁻¹	deci	d
10 ⁻²	centi	c
10 ⁻³	milli	m
10 ⁻⁶	micro	μ
10 ⁻⁹	nano	n
10 ⁻¹²	pico	p
10 ⁻¹⁵	femto	f

$$\text{lbs/day} = \text{MGD} * \text{mg/L} * 8.34$$

1 ppm = 1 mg/L for aqueous solutions

zero order reaction $C = C_0 - kt$

1st order reaction $\ln C = \ln C_0 - kt$ or $\ln \frac{C}{C_0} = -kt$ or $\frac{C}{C_0} = e^{-kt}$

Half life for 1st order reactions = $0.693 / k$ where k is reaction rate

Detention Time $t_d = V/Q$

First Order reactions

a) Batch Reactor $C = C_0 e^{-kt}$ or $\ln(C/C_0) = -kt$

b) CMFR $C = \frac{C_0}{1 + kt_d}$

c) For n identical (same V and t_d) CMFR

$$C_n = \frac{C_0}{(1 + kt_d)^n}$$

Tracer Flushing if tracer is mixed in the reactor and is being purged by a clean media $C = C_0 e^{-t/t_d}$

Tracer Flushing if tracer is entering a reactor with clean media and is being purged out $C = C_0 (1 - e^{-t/t_d})$

Area of a circle = $\pi d^2/4$ where d = diameter

7.48 Gallons = 1ft^3 3.78 L = 1 Gallon

Hydraulic loading = $Q/\text{Surface area of reactor}$

BOD_t = Ultimate BOD (1 - e^{-kt})

$k_t = k_{20} \Theta^{T-20}$ $\Theta = 1.135$ for 4-20°C and 1.056 for 20-30°C

Disinfection $N_t = N_0 e^{-kt}$ where N_0 initial bacteria concentration; N_t final bacteria concentration

Power $G^2 = P/\mu V$

Molecular Weights

C	12
H	1
O	16
N	14
Cl	35.5
S	32
Fe	56

GAS TRANSFER KINETICS

$\ln(C^* - C_t) = \ln(C^* - C_0) - K_L a t$ where

C^* = saturation concentration of oxygen in water (mass/volume)

C_t = oxygen concentration in water at ant time t (mass/volume)

$K_L a$ = gas transfer coefficient (time⁻¹)

t = time